



# PACECCS

Modelling blowdown of a long CCS dense phase pipeline using Symmetry Dynamics

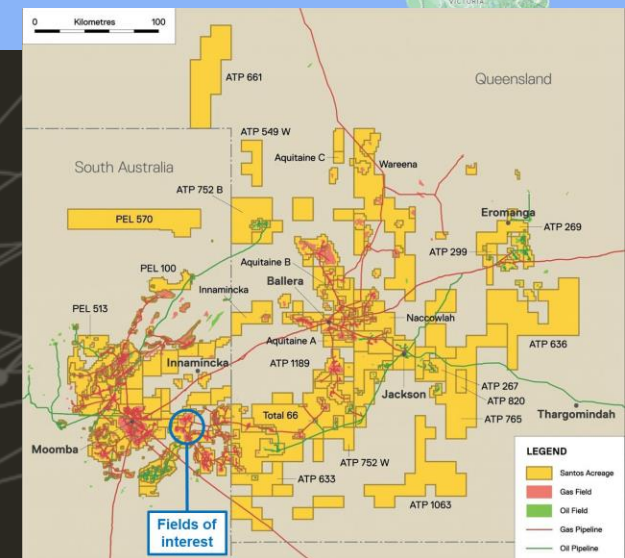
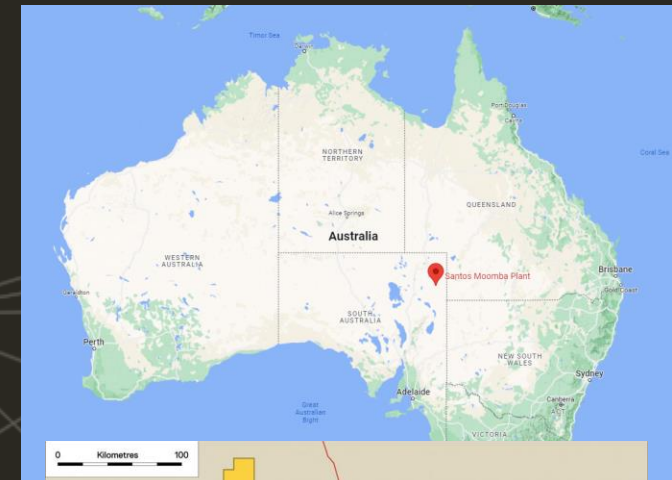
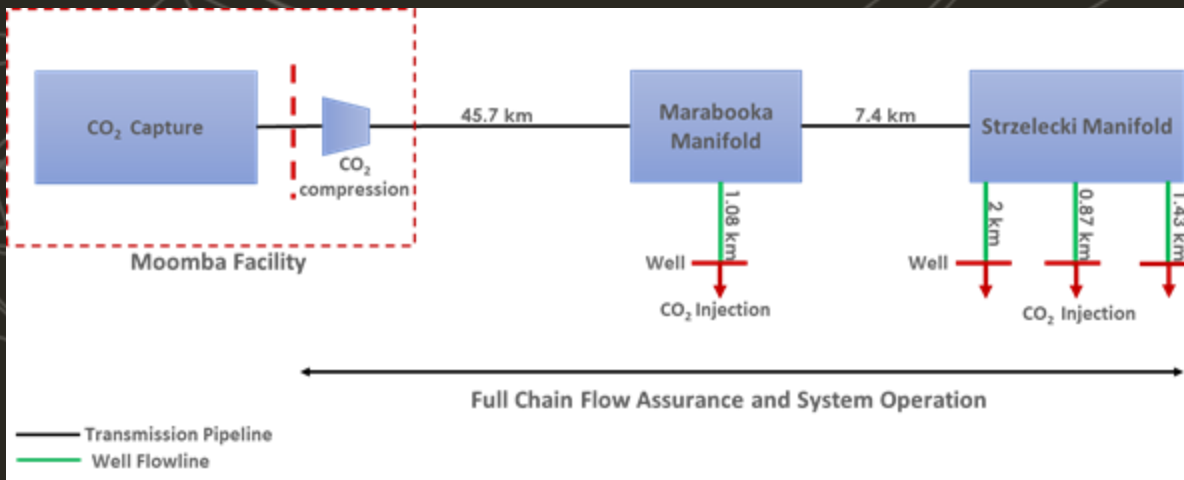
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# Cooper Basin Moomba CCS Project

- Capture 1.7 MTPA CO<sub>2</sub> from Moomba Gas Plant and sequester in depleted gas reservoirs in Cooper Basin
- Dense phase CO<sub>2</sub> transmission ~ 50km pipeline and 4 injection wells





# CCS Pipeline Depressurisation

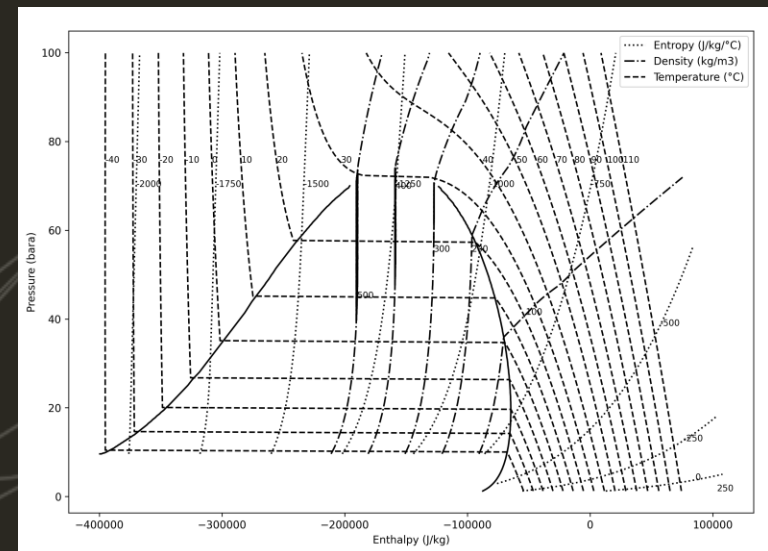
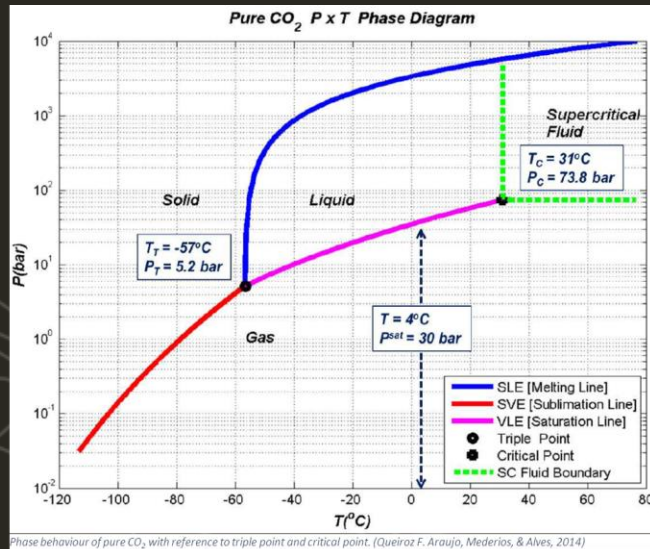


- Depressurisation is defined as the controlled disposal of pressurised fluids to a flare or vent system
- Systems are depressured for maintenance or in an emergency from operating pressure to atmospheric pressure
- Fairly simple and routine procedure in natural gas pipeline
- Much more complicated in CCS...



# CO<sub>2</sub> Joule-Thomson Effect

- JT cooling refers to the drop in temperature that occurs when a gas such as CO<sub>2</sub> expands from high pressure to low pressure at constant enthalpy



- JT coefficient of CO<sub>2</sub> is much higher than O&G fluids, therefore significantly larger temperature drops when depressuring down to -88°C
- Full depressurisation will lead to excessive JT cooling with the risk of solid CO<sub>2</sub> “snow”
- Freezing water will occur if the water dewpoint is reached



# Why is this a problem?

- Pipeline normal operating conditions ~146 barg
- Low temperatures during depressurization down to -88°C
- Material selection to design for all scenarios at extreme ends of design becomes very expensive

## Challenge:

- Review system to see if any mitigations exist to allow for the selection of a piping spec that does not need to cater for both extremes.

## Solution:

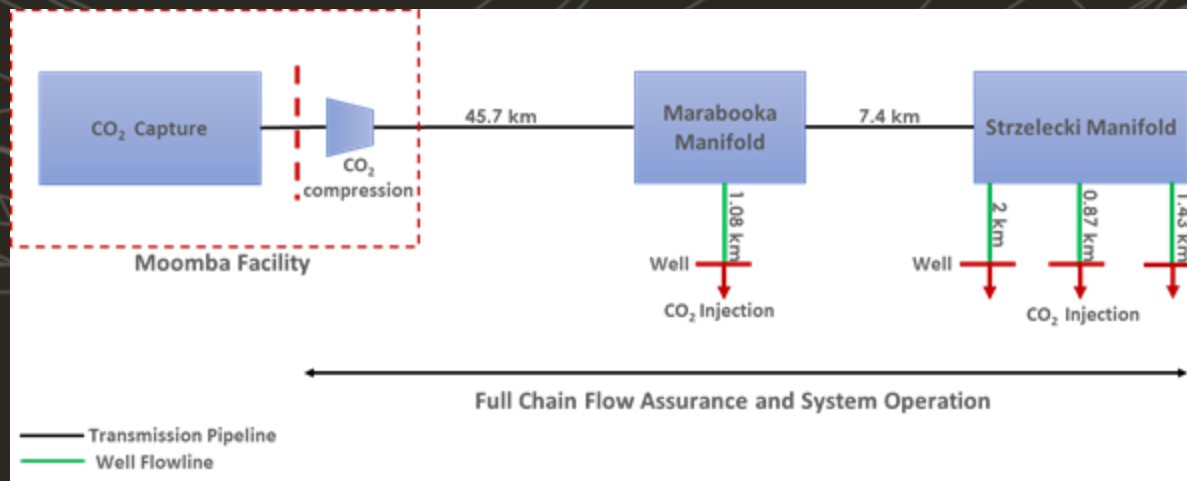
- Use of Schlumberger's Symmetry Dynamics to develop dynamic simulation of blowdown procedure
- Determine what the minimum metal temperature of piping and corresponding pressures will be



# Case Study - Proposed Solution

## Step 1

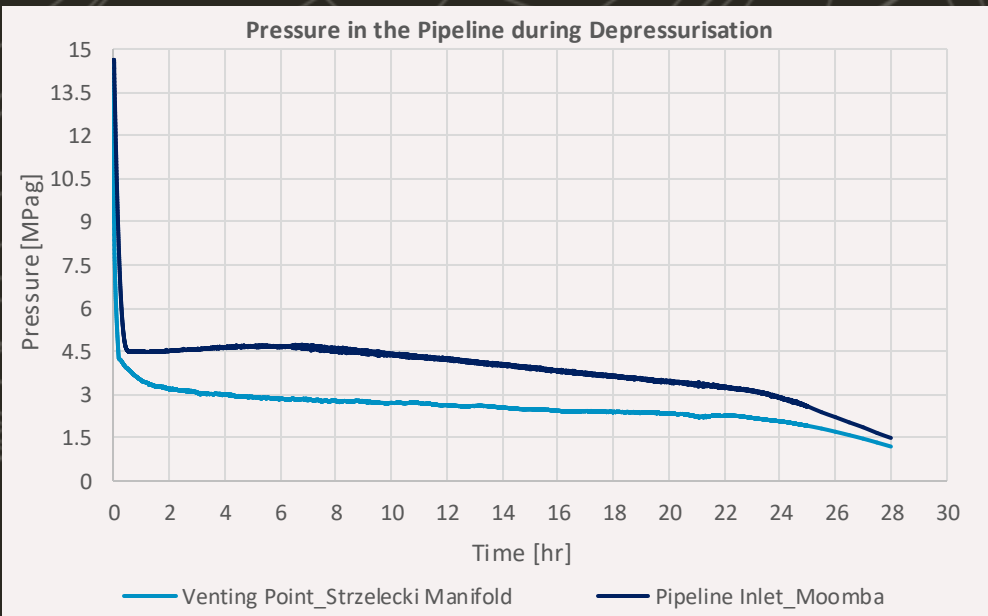
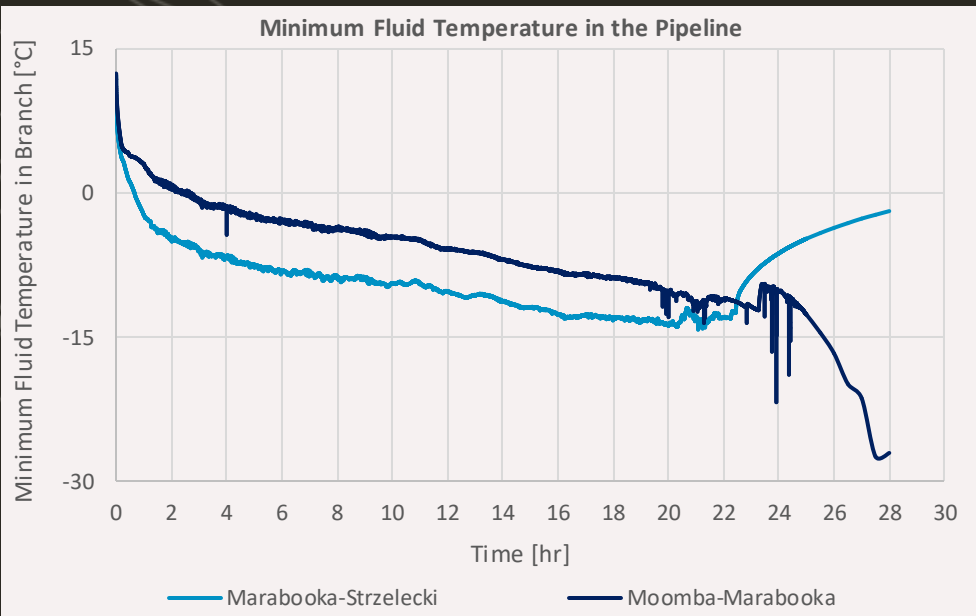
- Dissipate as much pressure as possible into the injection wells – pipeline pressure reduced from 146 barg to 80 barg
- Advantages:
  - Lower pressure starting point for full depressurization results in less JT cooling effects
  - Blowdown system only needs to be designed for 80 barg pressures
  - Sequester as much CO<sub>2</sub> as possible





# Case Study – Upstream of Blowdown Valve

- In 28 hours the minimum temperature seen in the pipeline at any point in time is  $-27^{\circ}\text{C}$
- Minimum temperature occurs in the Moomba-Marabooka section and it occurs towards the end of the depressurisation
- The location of the minimum temperature changes over time. The absolute lowest temperature occurs around 1-1.5 km from the Moomba station

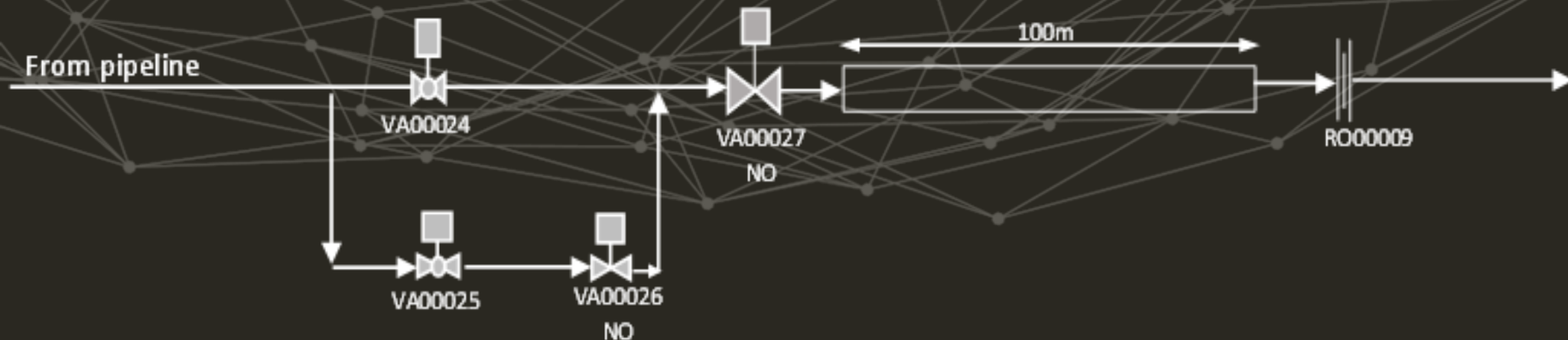
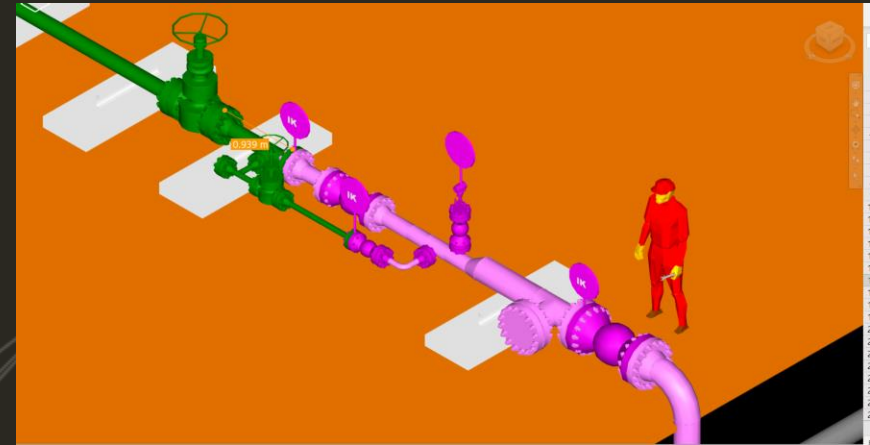




# Case Study - Proposed Solution

## Step 2

- Controlled blowdown over prolonged period of time to manage JT cooling impact
- Process Pressure : 80 bar (max operating 146 bar)
- Process Temperature : 25°C (winter) 55°C (summer)
- Blowdown valve size: 6"
- Restriction orifice size: 50mm

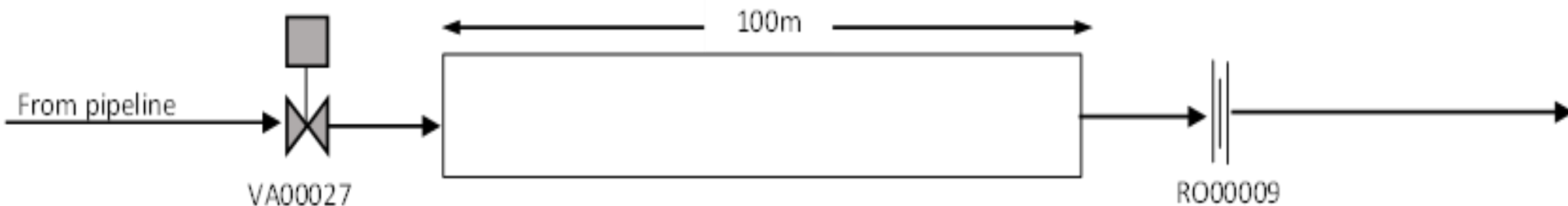






# Case Study - Modelling Challenge

- Carbon steel has a limit of  $-45^{\circ}\text{C}$  for pressures up to 153.2 bar
- Where is the cut off point for using carbon steel within the blowdown system?
- Modelling in Symmetry Dynamics can show us how the wall temperature will change at each segment along the blowdown line





# Case Study - Building the Model

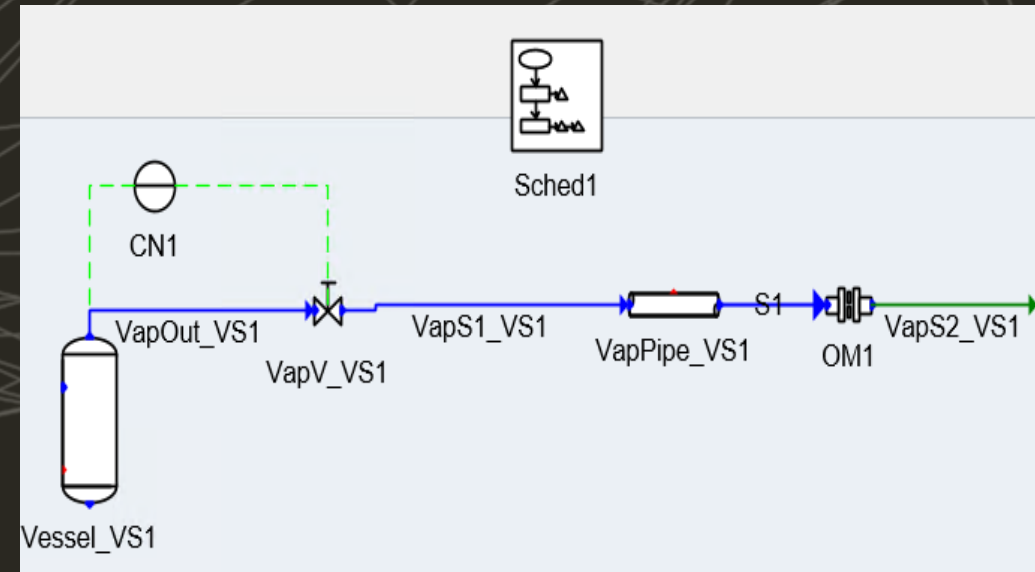
- System volume = 2356m<sup>3</sup>
- The pipe between the blowdown valve and the restriction orifice is 100m
- Blowdown valve is open by 10% until the system is pressurized before being fully open
- Summer process (55°C) case not modelled as the winter case of (25°C) presents worst case for low piping temperatures.

## Assumptions

- 6" Blowdown valve VA00027 opens linearly
- Valve opening is ramping opening (0.33%/s)

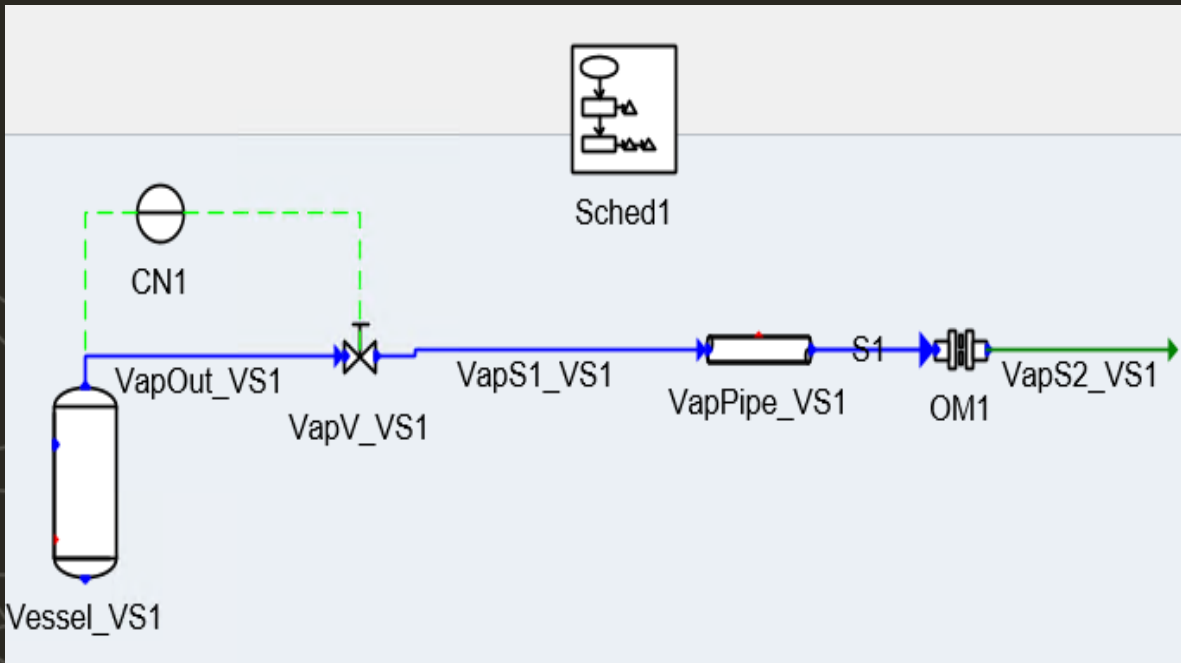
## Aim

- Identify a valve size that allows downstream piping to stay within CS limits





# Case Study – Dynamic Control



/FLDepS.CN1 (Dynamics - Controller)

OK

Name **CN1**

PV VapOut\_VS1.Mass Flow → OP VapV\_VS1.% Opening

SP [ ]

Summary Alarms Notes

Performance	
Name	Value
PV [kg/h]	0.00
SP [kg/h]	0.00
OP [%]	0.00

Tuning / Var Range	
Name	Value
Kc	0.5000
Ti [min]	0.50
Td [min]	0.50
PV Range	
PV Min [kg/h]	0.00
PV Max [kg/h]	10000.00
OP Range	
OP Min [%]	0.00
OP Max [%]	100.00

Settings	
Mode	Manual
Action	Reverse
Advanced	
Split Range	
Ramping	
Ramping Active	<input checked="" type="checkbox"/>
Ramp Time [min]	60.00
Ramp Mode	Output
Lock Ramping	<input type="checkbox"/>
OP Target [%]	
Rate Limit [%/s]	0.3330
Filtering	
FeedForward	
Auto Tuning	
Malfunctions	
Gain Scheduling	

/FLDepS.Sched1 (Dynamics - Scheduler)

Name **Sched1** Description

OK

Sequence Start/Stop Pause/Resume

Name	Completion	State
<b>Sequence</b>	Reset	Active

Events

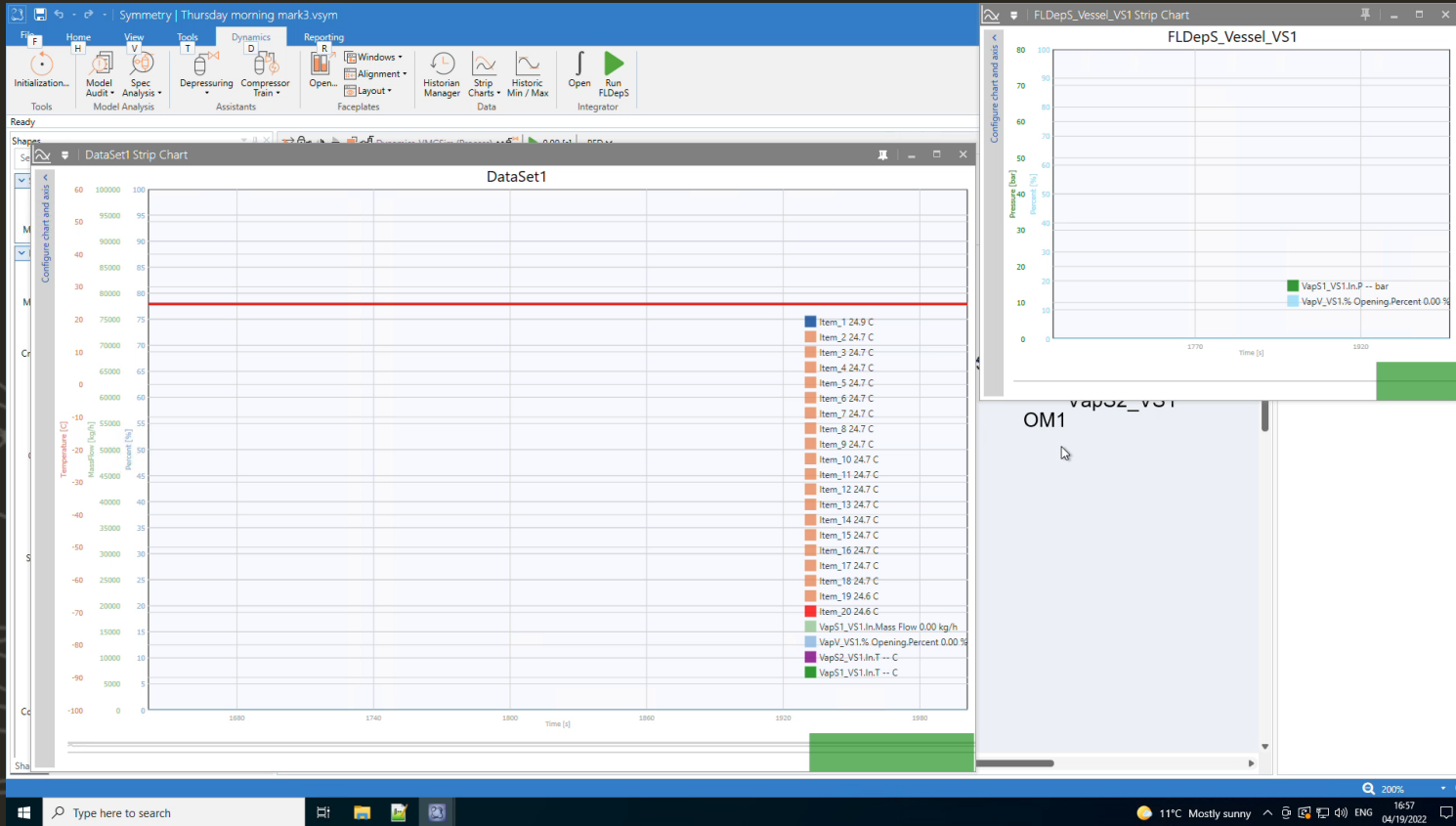
Name	Wait For	Wait Left	Or/And	Var Name	Current Value	Condition
1	<b>Wait_30s</b>	30.00 [s]	0.00 [s]	Or		
2	<b>Open_valve_10%</b>	0.00 [s]	0.00 [s]	Or		
3	<b>Valve_stays_open</b>	570.00 [s]	0.00 [s]	And	/FLDepS.VapV_VS1.%Opening	0.00 [%] Greater c
4	<b>Valve_opens_to_100%</b>	30.00 [s]	0.00 [s]	Or		

Sequence

- Wait\_30s
- Open\_valve\_10%
  - Action
- Valve\_stays\_open
- Valve\_opens\_to\_100%
  - Action

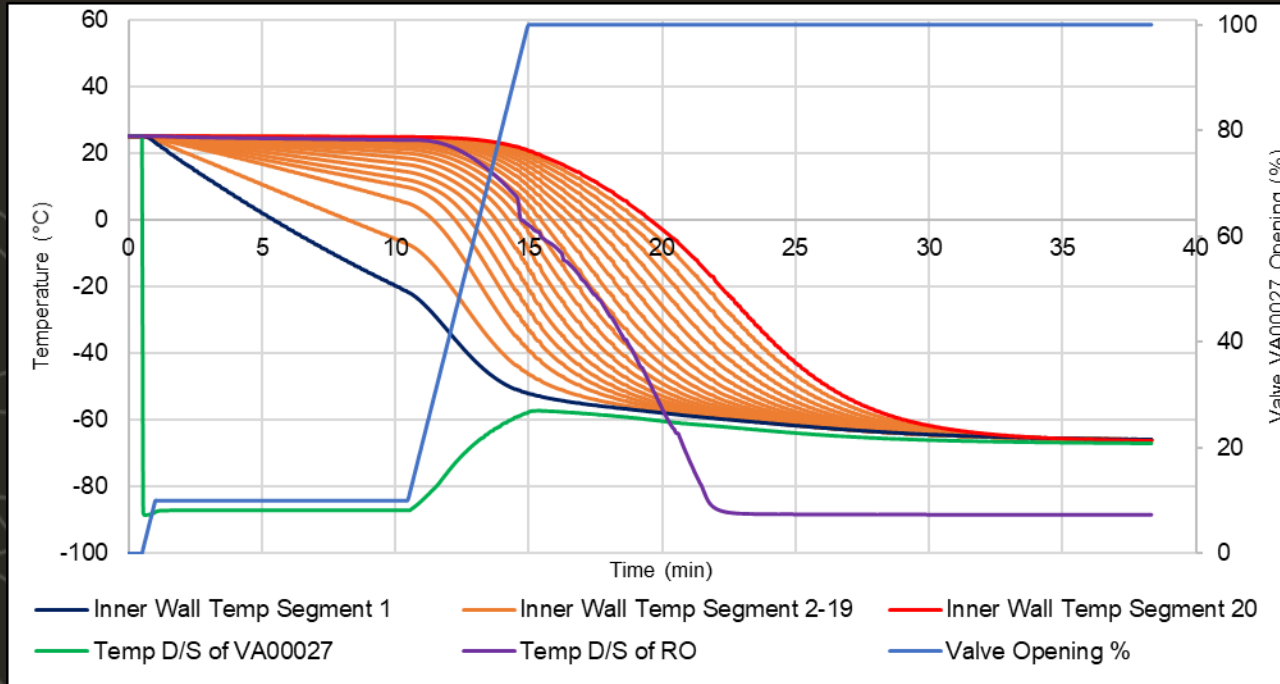


# Case Study – Dynamics Running



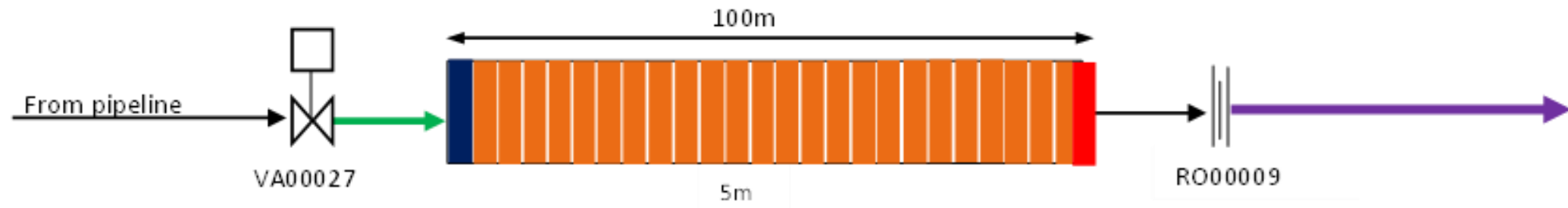


# Case Study - Small Control Valve



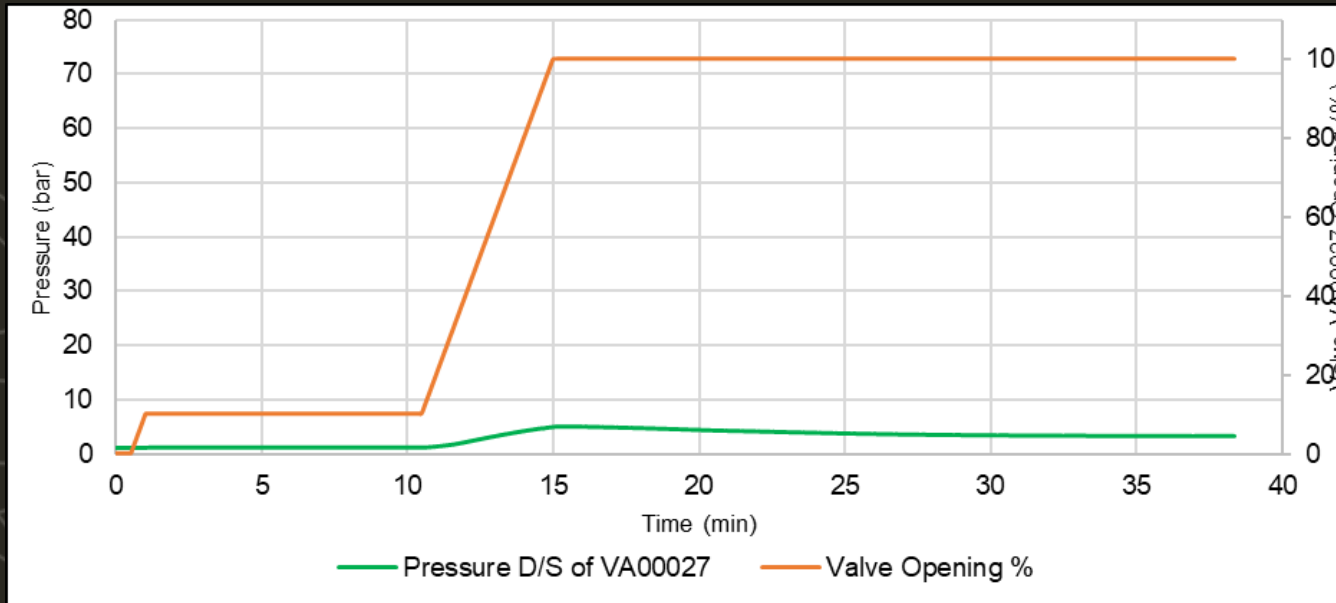
Temperature profiles for a valve Cv of 2  
Operating conditions of 80barg and 25°C

Piping wall breaches the -45°C limit  
The piping wall temperature (orange) is -60°C



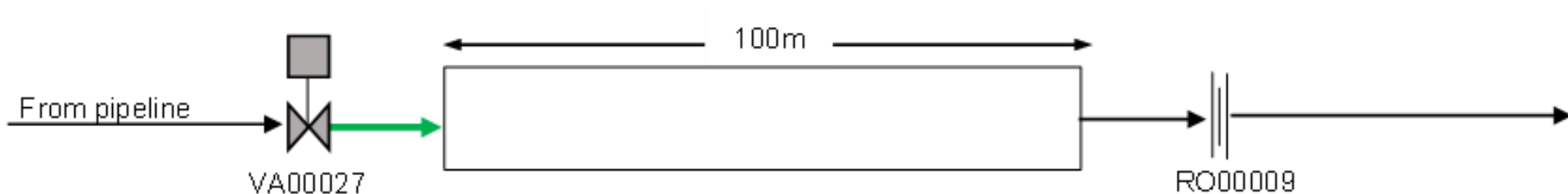


# Case Study - Small Control Valve



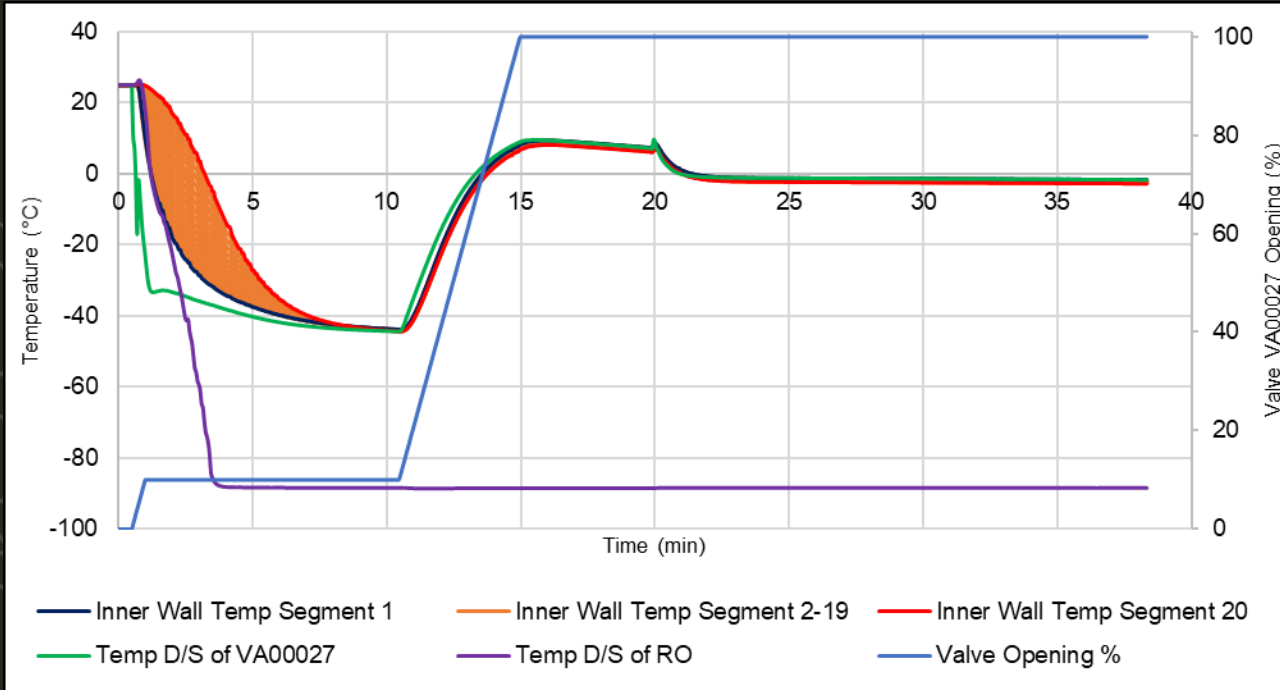
Pressure profiled for a valve  
CV of 2  
Operating conditions of  
80 barg and 25°C

Maximum pressure (green)  
is 5 bar  
After 24hrs the pressure of  
the system is 69 bar



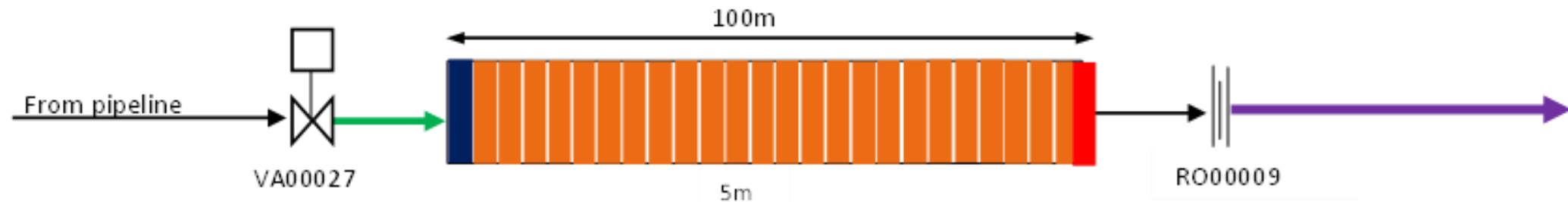


# Case Study - Optimum Control Valve Size



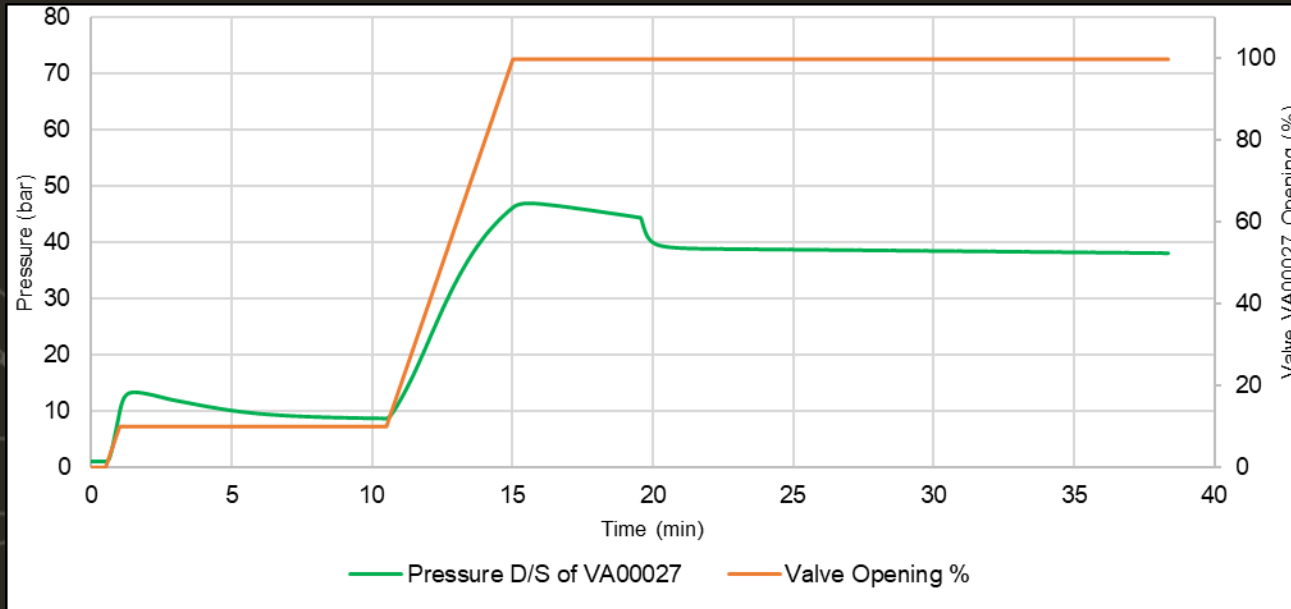
Temperature profiles for a valve CV of 53  
Operating conditions of 80barg and 25°C

Process fluid temperature (green) lowest is -43°C  
The piping wall temperature (orange) is -44°C



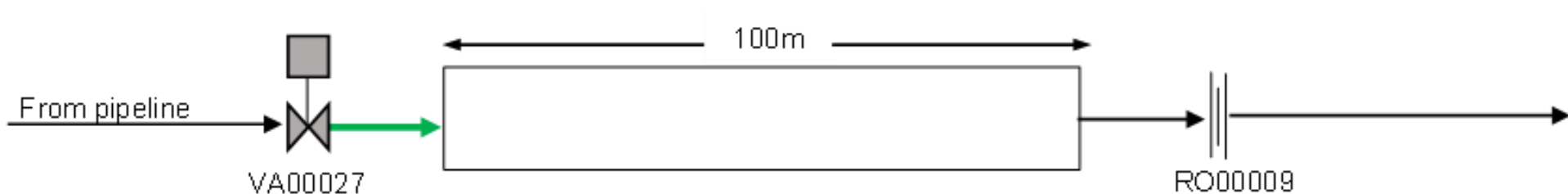


# Case Study - Optimum Control Valve Size



Pressure profiled for a valve CV of 53  
Operating conditions of 80 barg and 25°C

Maximum pressure (green) is 47 bar  
After 24hrs the pressure of the system is 36.6 bar  
Complete depressurisation takes place after 48 hours

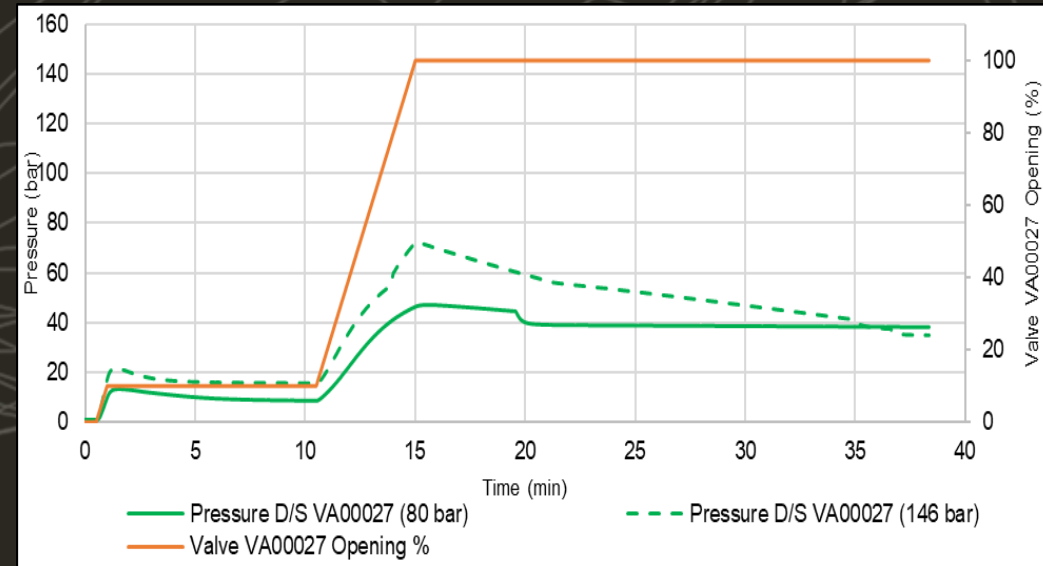
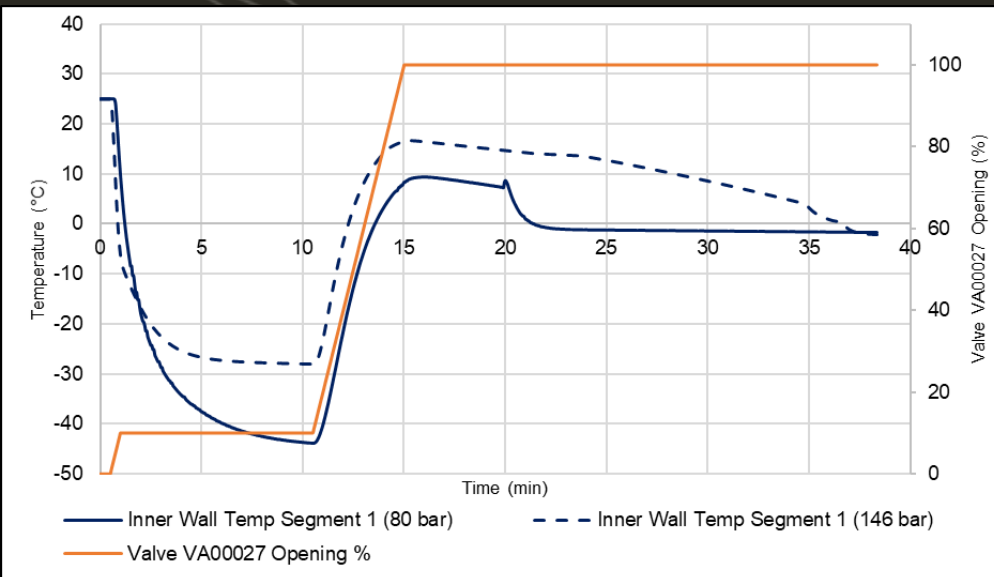






# Case Study - Pressure Sensitivity

- Max operating pressure 146 bar vs 80bar
- Operating temperature 25°C
- Lower operating pressure for the same valve Cv results in the worst case for low piping wall temperatures
- Higher operating pressure for the same valve Cv results in the worst case for maximum pressure downstream the valve





# Case Study – Project Recommendations

- Two stage depressurisation required
- Maximum blowdown valve size of Cv 53 & RO size 50mm
- Minimum piping wall temperature downstream of blowdown valve -44°C
- Maximum pressure seen downstream of blowdown valve 47 barg
- Entire duration of second stage of blowdown (from 80 to 0 barg) to take 48 hours



# Case Study – Conclusions

- Using Schlumberger's Symmetry Dynamics we were able to provide a solution to the project with confidence that carbon steel minimum design temperatures would not be breached.
- Design conditions of blowdown system reduced:
  - Before: 146 barg and -88°C
  - After: 46 barg and -44°C
- Enabled significant cost savings to the project not requiring expensive specialist materials
- Added benefit of Symmetry Dynamics was being able to perform blowdown valve sizing



**PACE**